Economic Commission for Europe

Inland Transport Committee

Working Party on the Transport of Dangerous Goods

Joint Meeting of Experts on the Regulations annexed to the

European Agreement concerning the International Carriage

of Dangerous Goods by Inland Waterways (ADN)

(ADN Safety Committee)

Twenty-eighth session

Geneva, 25-29 January 2016

Item 5 (b) of the provisional agenda

Proposals for amendments to the Regulations annexed to ADN:

Other proposals

 Proposal to add to Table C

 Transmitted by the Central Commission for the Navigation of the Rhine (CCNR)[[1]](#footnote-1)

1. This question has arisen because it was noted that the various language versions of ADN differed for UN No. 1268 PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. Following the discussion, it was found that there were similar problems for UN No. 1267 PETROLEUM CRUDE OIL, UN No. 1863 FUEL, AVIATION, TURBINE ENGINE, UN No. 1993 FLAMMABLE LIQUID, N.O.S. and UN No. 3295 HYDROCARBONS, LIQUID, N.O.S. None of the versions were completely coherent.

2. Other problems emerged owing to the wording of remark 38 in Table C, which no longer corresponds with the current content of the requirements. It refers to the conditions applicable for packing group II, while there are already entries for packing group II.

3. The informal working group considered this problem on numerous occasions and concluded that three situations were possible:

 (a) Carriage is on a type C vessel. All the data for the calculation of the pressurization of the tank is available. The conditions of transport can be determined using scheme A of the decision tree;

 (b) Carriage is on a type C vessel. Not all the data for the calculation of the pressurization of the tank is available (some is missing). The conditions of transport are determined by referring to ranges of initial boiling points (decision tree, scheme A, fourth column);

 (c) Carriage is on a type N closed vessel. The vapour pressure at 50° C determines the conditions of transport (decision tree, scheme B).

4. The method for determining the initial boiling point in accordance with ASTMD 86-01 produces higher values because of the test conditions in the low temperature ranges. This is important from the point of view of safety for initial boiling points near 60° C, the limit for carriage in a pressure tank. That is why for initial boiling points over 60° C and equal to or under 85° C, if the calculation has been done in accordance with ASTMD 86-01, the carriage should just the same be carried out in a pressure tank.

5. For situation (a), above, references are required for packing groups I, II and III, without any information additional to the name or designation. A reference makes it possible to specify that the use of the decision tree is required to determine the conditions of transport.

6. For situation (b) (with data missing), the following references are required:

| *Packing group* | *Information additional to the name or designation* | *Conditions of transport* |
| --- | --- | --- |
|  |  |  |
| I | Initial boiling point ≤ 60° C | Pressure tank |
| II | Initial boiling point ≤ 60° C | Pressure tank |
|  | 60° C < initial boiling point ≤ 85° C | 50 kPa, with water spraying (remark 38) |
|  | 85° C < initial boiling point ≤ 115° C | 50 kPa |
|  | Initial boiling point > 115° C | 35 kPa |
| III | Initial boiling point ≤ 60° C | Pressure tank |
|  | 60° C < initial boiling point ≤ 85° C | 50 kPa, with water spraying (remark 38) |
|  | 85° C < initial boiling point ≤ 115° C | 50 kPa |
|  | Initial boiling point > 115° C | 35 kPa |

7. For situation (c) the following references are required:

| *Information additional to the name or designation* | *Conditions of transport* |
| --- | --- |
|  |  |
| 175 kPa ≤ Pd 50 < 300 kPa | Pressure tank |
| 175 kPa ≤ Pd 50 < 300 kPa | 50 kPa with refrigeration |
| 110 kPa ≤ Pd 50 < 175 kPa | 50 kPa |
| 110 kPa ≤ Pd 50 < 150 kPa | 10 kPa with water spraying |
| Pd 50 < 110 kPa | 10 kPa |

8. It is proposed to amend the wording of remark 38 in 3.2.3.1, Column (20), which leads to confusion owing to the current content of the requirements, and to recast the remark as follows:

“38. For an initial boiling point above 60° C and under or equal to 85° C as determined in accordance with ASTMD 86-01, the applicable conditions of transport are identical with those stipulated for an initial boiling point under or equal to 60° C.”

9. Furthermore, it is proposed to add to the wording in 3.2.3.3 Column (20) and in 3.2.4.3 L Column (20) so that it reads as follows:

“38. Reference must be made in column (20) to remark 38 for mixtures with an initial boiling point above 60º C or under or equal to 85º C in accordance with ASTMD 86-01.”

10. For Table C it is proposed to delete any mention of UN Nos. 1267, 1268, 1863, 1993 and 3295 and to add the following lines in Table C. Pursuant to the recommendation of the informal working group on substances, “(N1, N2 or N3)” was added to Column (5), “Dangers”, for all entries with the name or designation “WITH MORE THAN 10% BENZENE”.

| *UN No. or substance identification No.* | *Name and description* | *Class* | *Classification code* | *Packing group* | *Dangers* | *Type of tank vessel* | *Cargo tank design* | *Cargo tank type* | *Cargo tank equipment* | *Opening pressure of the high-velocity vent valve in kPa* | *Maximum degree of filling in%* | *Relative density at 20° C* | *Type of sampling device* | *Pump room below deck permitted* | *Temperature class* | *Explosion group* | *Anti-explosion protection required* | *Equipment required* | *Number of cones/blue lights* | *Additional requirements/Remarks* |
| --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- |
| *(1)* | *(2)* | *(3a)* | *(3b)* | *(4)* | *(5)* | *(6)* | *(7)* | *(8)* | *(9)* | *(10)* | *(11)* | *(12)* | *(13)* | *(14)* | *(15)* | *(16)* | *(17)* | *(18)* | *(19)* | *(20)* |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| 1267 | PETROLEUM CRUDE OIL | 3 | F1 | I | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |  | \* | yes | T43) | II B4) | yes | \* | 1 | 14;\*see 3.2.3.3 |
| 1267 | PETROLEUM CRUDE OIL | 3 | F1 | II | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |  | \* | yes | T43) | II B4) | yes | \* | 1 | 14;\*see 3.2.3.3 |
| 1267 | PETROLEUM CRUDE OIL | 3 | F1 | III | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |  | \* | yes | T43) | II B4) | yes | \* | 0 | 14;\*see 3.2.3.3 |
| 1267 | PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENEINITIAL BOILING POINT ≤ 60° C | 3 | F1 | I | 3+CMR+F+(N1, N2, N3) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 1267 | PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENEINITIAL BOILING POINT ≤ 60° C | 3 | F1 | II | 3+CMR+F+(N1, N2, N3) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 1267 | PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE60° C < INITIAL BOILING POINT ≤ 85° C | 3 | F1 | II | 3+CMR+F+(N1, N2, N3) | C | 2 | 2 | 3 | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 23; 29; 38 |
| 1267 | PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE85° C < INITIAL BOILING POINT ≤ 115° C | 3 | F1 | II | 3+CMR+F+(N1, N2, N3) | C | 2 | 2 |  | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 1267 | PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENEINITIAL BOILING POINT > 115° C | 3 | F1 | II | 3+CMR+F+(N1, N2, N3) | C | 2 | 2 |  | 35 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 1267 | PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENEINITIAL BOILING POINT ≤ 60° C | 3 | F1 | III | 3+CMR+F+(N1, N2, N3) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 29 |
| 1267 | PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE60° C < INITIAL BOILING POINT ≤ 85° C | 3 | F1 | III | 3+CMR+F+(N1, N2, N3) | C | 2 | 2 | 3 | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 23; 29; 38 |
| 1267 | PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENE85° C < INITIAL BOILING POINT ≤ 115° C | 3 | F1 | III | 3+CMR+F+(N1, N2, N3) | C | 2 | 2 |  | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 29 |
| 1267 | PETROLEUM CRUDE OIL WITH MORE THAN 10% BENZENEINITIAL BOILING POINT > 115° C | 3 | F1 | III | 3+CMR+F+(N1, N2, N3) | C | 2 | 2 |  | 35 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 29 |
| 1268 | PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. | 3 | F1 | I | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |   | \* | yes | T43) | II B4) | yes | \* | 1 | 14; 27\*see 3.2.3.3 |
| 1268 | PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. | 3 | F1 | II | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |   | \* | yes | T43) | II B4) | yes | \* | 1 | 14; 27\*see 3.2.3.3 |
| 1268 | PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. | 3 | F1 | III | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |  | \* | yes | T43) | II B4) | yes | \* | 0 | 14; 27\*see 3.2.3.3 |
| 1268 | PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. WITH MORE THAN 10% BENZENEINITIAL BOILING POINT ≤ 60° C | 3 | F1 | I | 3+CMR+F+(N1, N2, N3) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 27; 29 |
| 1268 | PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. WITH MORE THAN 10% BENZENEINITIAL BOILING POINT ≤ 60° C | 3 | F1 | II | 3+CMR+F+(N1, N2, N3) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 27; 29 |
| 1268 | PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. WITH MORE THAN 10% BENZENE60° C < INITIAL BOILING POINT ≤ 85° C | 3 | F1 | II | 3+CMR+F+(N1, N2, N3) | C | 2 | 2 | 3 | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 23; 27; 29; 38 |
| 1268 | PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. WITH MORE THAN 10% BENZENE85° C < INITIAL BOILING POINT ≤ 115° C | 3 | F1 | II | 3+CMR+F+(N1, N2, N3) | C | 2 | 2 |  | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 27; 29 |
| 1268 | PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S. WITH MORE THAN 10% BENZENEINITIAL BOILING POINT > 115° C | 3 | F1 | II | 3+CMR+F+(N1, N2, N3) | C | 2 | 2 |  | 35 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 27; 29 |
| 1268 | PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S.(NAPHTA) 110 kPa < vp50 ≤ 175 kPa | 3 | F1 | II | 3+N2+CMR+F | N | 2 | 3 |  | 50 | 97 | 0,735 | 3 | yes | T3 | II A | yes | PP, EP, EX, TOX, A | 1 | 14; 29 |
| 1268 | PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S.(NAPHTA) 110 kPa < vp50 ≤ 150 kPa | 3 | F1 | II | 3+N2+CMR+F | N | 2 | 3 | 3 | 10 | 97 | 0,735 | 3 | yes | T3 | II A | yes | PP, EP, EX, TOX, A | 1 | 14; 29 |
| 1268 | PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S.(NAPHTA) vp50 ≤ 110 kPa | 3 | F1 | II | 3+N2+CMR+F | N | 2 | 3 |  | 10 | 97 | 0,735 | 3 | yes | T3 | II A | yes | PP, EP, EX, TOX, A | 1 | 14; 29 |
| 1268 | PETROLEUM DISTILLATES, N.O.S. or PETROLEUM PRODUCTS, N.O.S(BENZENE HEART CUT) vp50 ≤ 110 kPa | 3 | F1 | II | 3+N2+CMR+F | N | 2 | 3 |  | 10 | 97 | 0,765 | 3 | yes | T3 | II A | yes | PP, EP, EX, TOX, A | 1 | 14; 29 |
| 1863 | FUEL, AVIATION, TURBINE ENGINE | 3 | F1 | I | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |   | \* | yes | T43) | II B4) | yes | \* | 1 | 14;\*see 3.2.3.3 |
| 1863 | FUEL, AVIATION, TURBINE ENGINE | 3 | F1 | II | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |   | \* | yes | T43) | II B4) | yes | \* | 1 | 14;\*see 3.2.3.3 |
| 1863 | FUEL, AVIATION, TURBINE ENGINE | 3 | F1 | III | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |   | \* | yes | T43) | II B4) | yes | \* | 0 | 14;\*see 3.2.3.3 |
| 1863 | FUEL, AVIATION, TURBINE ENGINE WITH MORE THAN 10% BENZENEINITIAL BOILING POINT ≤ 60° C | 3 | F1 | I | 3+CMR+F+(N1, N2, N3) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 1863 | FUEL, AVIATION, TURBINE ENGINE WITH MORE THAN 10% BENZENEINITIAL BOILING POINT ≤ 60° C | 3 | F1 | II | 3+CMR+F+(N1, N2, N3) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 1863 | FUEL, AVIATION, TURBINE ENGINE WITH MORE THAN 10% BENZENE60° C < INITIAL BOILING POINT ≤ 85° C | 3 | F1 | III | 3+CMR+F+(N1, N2, N3) | C | 2 | 2 | 3 | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 23; 29; 38 |
| 1863 | FUEL, AVIATION, TURBINE ENGINE WITH MORE THAN 10% BENZENE85° C < INITIAL BOILING POINT ≤ 115° C | 3 | F1 | III | 3+CMR+F+(N1, N2, N3) | C | 2 | 2 |  | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 29 |
| 1863 | FUEL, AVIATION, TURBINE ENGINE WITH MORE THAN 10% BENZENEINITIAL BOILING POINT > 115° C | 3 | F1 | III | 3+CMR+F+(N1, N2, N3) | C | 2 | 2 |  | 35 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 29 |
| 1993 | FLAMMABLE LIQUID, N.O.S. | 3 | F1 | I | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |   | \* | yes | T43) | II B4) | yes | \* | 1 | 14;\*see 3.2.3.3 |
| 1993 | FLAMMABLE LIQUID, N.O.S. | 3 | F1 | II | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |   | \* | yes | T43) | II B4) | yes | \* | 1 | 14;\*see 3.2.3.3 |
| 1993 | FLAMMABLE LIQUID, N.O.S. | 3 | F1 | III | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |   | \* | yes | T43) | II B4) | yes | \* | 0 | 14;\*see 3.2.3.3 |
| 1993 | FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENEINITIAL BOILING POINT ≤ 60° C | 3 | F1 | I | 3+(N1, N2, N3, CMR, F) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 1993 | FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENEINITIAL BOILING POINT ≤ 60° C | 3 | F1 | II | 3+(N1, N2, N3, CMR, F) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 1993 | FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE60° C < INITIAL BOILING POINT ≤ 85° C | 3 | F1 | II | 3+(N1, N2, N3, CMR, F) | C | 2 | 2 | 3 | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 23; 29; 38 |
| 1993 | FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE85° C < INITIAL BOILING POINT ≤ 115° C | 3 | F1 | II | 3+(N1, N2, N3, CMR, F) | C | 2 | 2 |  | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 1993 | FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENEINITIAL BOILING POINT > 115° C | 3 | F1 | II | 3+(N1, N2, N3, CMR, F) | C | 2 | 2 |  | 35 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 1993 | FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENEINITIAL BOILING POINT ≤ 60° C | 3 | F1 | III | 3+(N1, N2, N3, CMR, F) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 29 |
| 1993 | FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE60° C < INITIAL BOILING POINT ≤ 85° C | 3 | F1 | III | 3+(N1, N2, N3, CMR, F) | C | 2 | 2 | 3 | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 23; 29; 38 |
| 1993 | FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENE85° C < INITIAL BOILING POINT ≤ 115° C | 3 | F1 | III | 3+(N1, N2, N3, CMR, F) | C | 2 | 2 |  | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 29 |
| 1993 | FLAMMABLE LIQUID, N.O.S. WITH MORE THAN 10% BENZENEINITIAL BOILING POINT > 115° C | 3 | F1 | III | 3+(N1, N2, N3, CMR, F) | C | 2 | 2 |  | 35 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 29 |
| 1993 | FLAMMABLE LIQUID, N.O.S. (CYCLOHEXANONE/CYCLOHEXANOL MIXTURE) | 3 | F1 | III | 3+F | N | 3 | 3 |  |  | 97 | 0,95 | 3 | yes | T3 | II A | yes | PP,EX, A | 0 |  |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. | 3 | F1 | I | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |   | \* | yes | T43) | II B4) | yes | \* | 1 | 14;\*see 3.2.3.3 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. | 3 | F1 | II | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |   | \* | yes | T43) | II B4) | yes | \* | 1 | 14;\*see 3.2.3.3 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. | 3 | F1 | III | 3+(N1, N2, N3, CMR, F) | \* | \* | \* | \* | \* | \* |   | \* | yes | T43) | II B4) | yes | \* | 0 | 14;\*see 3.2.3.3 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C | 3 | F1 | I | 3+CMR+(N1, N2, N3) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C | 3 | F1 | II | 3+CMR+(N1, N2, N3) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE 60° C < INITIAL BOILING POINT ≤ 85° C | 3 | F1 | II | 3+CMR+(N1, N2, N3) | C | 2 | 2 | 3 | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 23; 29; 38 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE 85° C < INITIAL BOILING POINT ≤ 115° C | 3 | F1 | II | 3+CMR+(N1, N2, N3) | C | 2 | 2 |  | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT > 115°C | 3 | F1 | II | 3+CMR+(N1, N2, N3) | C | 2 | 2 |  | 35 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 1 | 29 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT ≤ 60° C | 3 | F1 | III | 3+CMR+(N1, N2, N3) | C | 1 | 1 |  |  | 95 |  | 1 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 29 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE 60° C < INITIAL BOILING POINT ≤ 85° C | 3 | F1 | III | 3+CMR+(N1, N2, N3) | C | 2 | 2 | 3 | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 23; 29; 38 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE 85° C < INITIAL BOILING POINT ≤ 115° C | 3 | F1 | III | 3+CMR+(N1, N2, N3) | C | 2 | 2 |  | 50 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 29 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. WITH MORE THAN 10% BENZENE INITIAL BOILING POINT > 115° C | 3 | F1 | III | 3+CMR+(N1, N2, N3) | C | 2 | 2 |  | 35 | 95 |  | 2 | yes | T43) | II B4) | yes | PP, EP, EX, TOX, A | 0 | 29 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. CONTAINING ISOPRENE AND PENTADIENE, STABILIZED[[2]](#footnote-2) | 3 | F1 | I | 3+inst.+N2+CMR | C | 2 | 2 | 3 | 50 | 95 | 0,678 | 1 | yes | T43) | II B4) | yes | PP,EX, A | 1 | 3; 27 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S.(1-OCTEN) | 3 | F1 | II | 3+N2+F | N | 2 | 3 |  | 10 | 97 | 0,71 | 3 | yes | T3 | II B4) | yes | PP, EP, EX, TOX, A | 1 | 14 |
| 3295 | HYDROCARBONS, LIQUID, N.O.S. (POLYCYCLIC AROMATIC HYDOCARBONS MIXTURE) | 3 | F1 | III | 3+CMR+F | N | 2 | 3 | 3 | 10 | 97 | 1,08 | 3 | yes | T1 | II A | yes | PP, EP, EX, TOX, A | 0 | 14 |

1. Distributed in German by the Central Commission for the Navigation of the Rhine under the symbol CCNR/ZKR/ADN/WP.15/AC.2/2016/2. [↑](#footnote-ref-1)
2. Possibly to be added: “60 °C < INITIAL BOILING POINT ≤ 85 °C” Remark 38, consequently with a line for INITIAL BOILING POINT ≤ 60 °C, i.e., pressure tank. [↑](#footnote-ref-2)