

What Do We Need for Cost-effective CCS

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F-T Process Development Unit.
2510 Research Park Drive

CAER Lab #2
2582 Research Park Drive

Minerals Processing Facility

Spindletop Administration Building
2624 Research Park Drive

CAER Lab #1
2540 Research Park Drive

Fiber Development Facility

Synthesis
& Pitch Lab

Algae Greenhouse

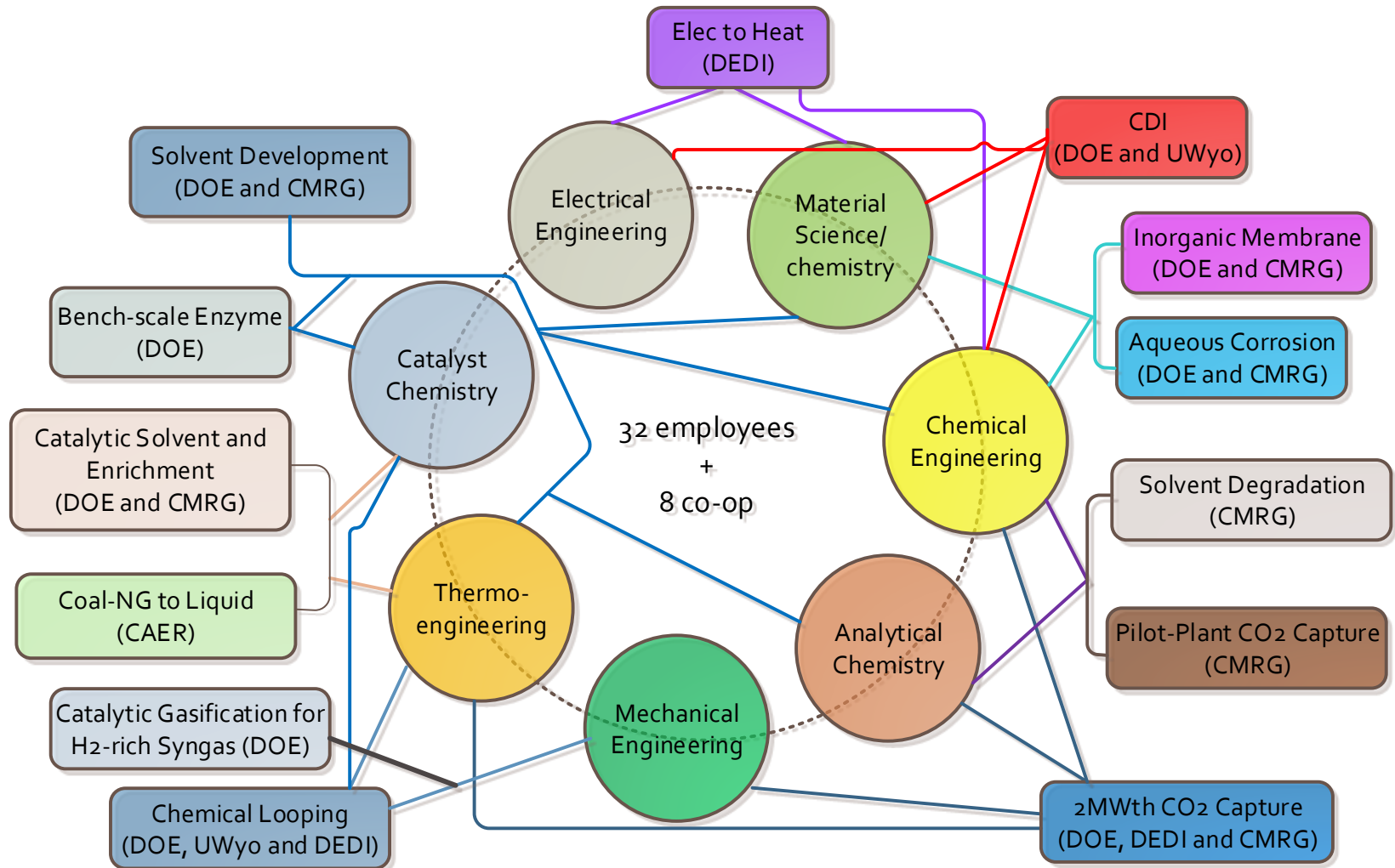
Industrial Support Facility

Research Divisions

- Biofuels and Environmental Catalysts
- Carbon Materials
- Clean Fuels and Chemicals
- Environmental and Coal Technology
- Electrochemical Power Sources
- Power Generation and Utility Fuels

Web: www.caer.uky.edu

Our Expertise and Projects on CCS



A large industrial facility, likely a refinery or chemical plant, featuring a complex network of steel scaffolding, stairs, and platforms. A white pickup truck is parked in the foreground, and a large storage tank is visible on the left.



Post Combustion Scrubbing in Fossil Power Plants

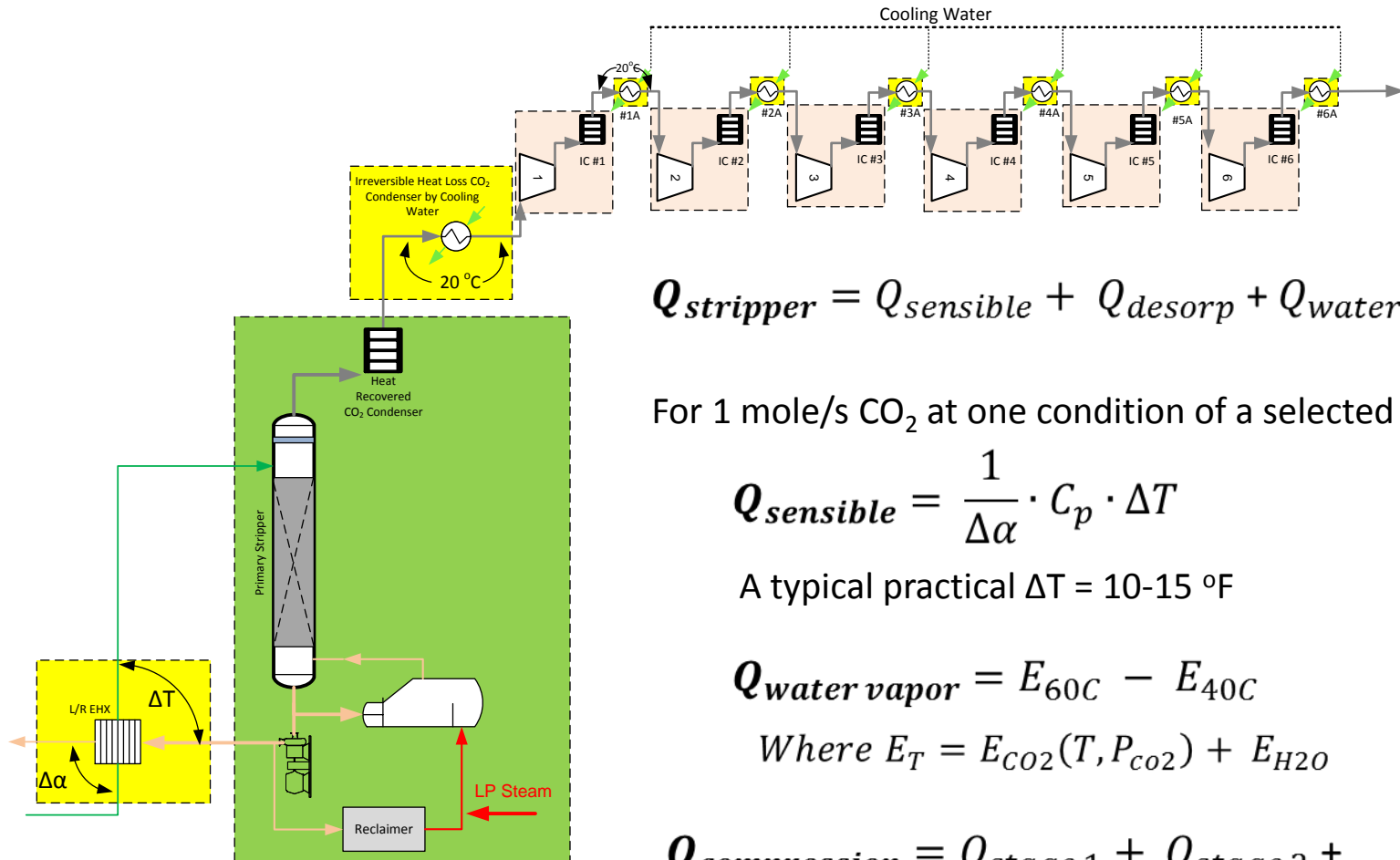
•Challenges:

- Low CO₂ partial pressure (~0.14 atm)
- Large volume
- Poisoning

•Consequences:

- Capital Costs \$700-1000/kW
- Absorbers three or four times diameter as FGD with packing
- Strippers and BOP
- 25-35% of plant output reduction

Minimum Energy Needed for Stripping and Compression for a Selected Solvent



$$Q_{stripper} = Q_{sensible} + Q_{desorp} + Q_{water\ vapor}$$

For 1 mole/s CO₂ at one condition of a selected solvent

$$Q_{sensible} = \frac{1}{\Delta\alpha} \cdot C_p \cdot \Delta T$$

A typical practical ΔT = 10-15 °F

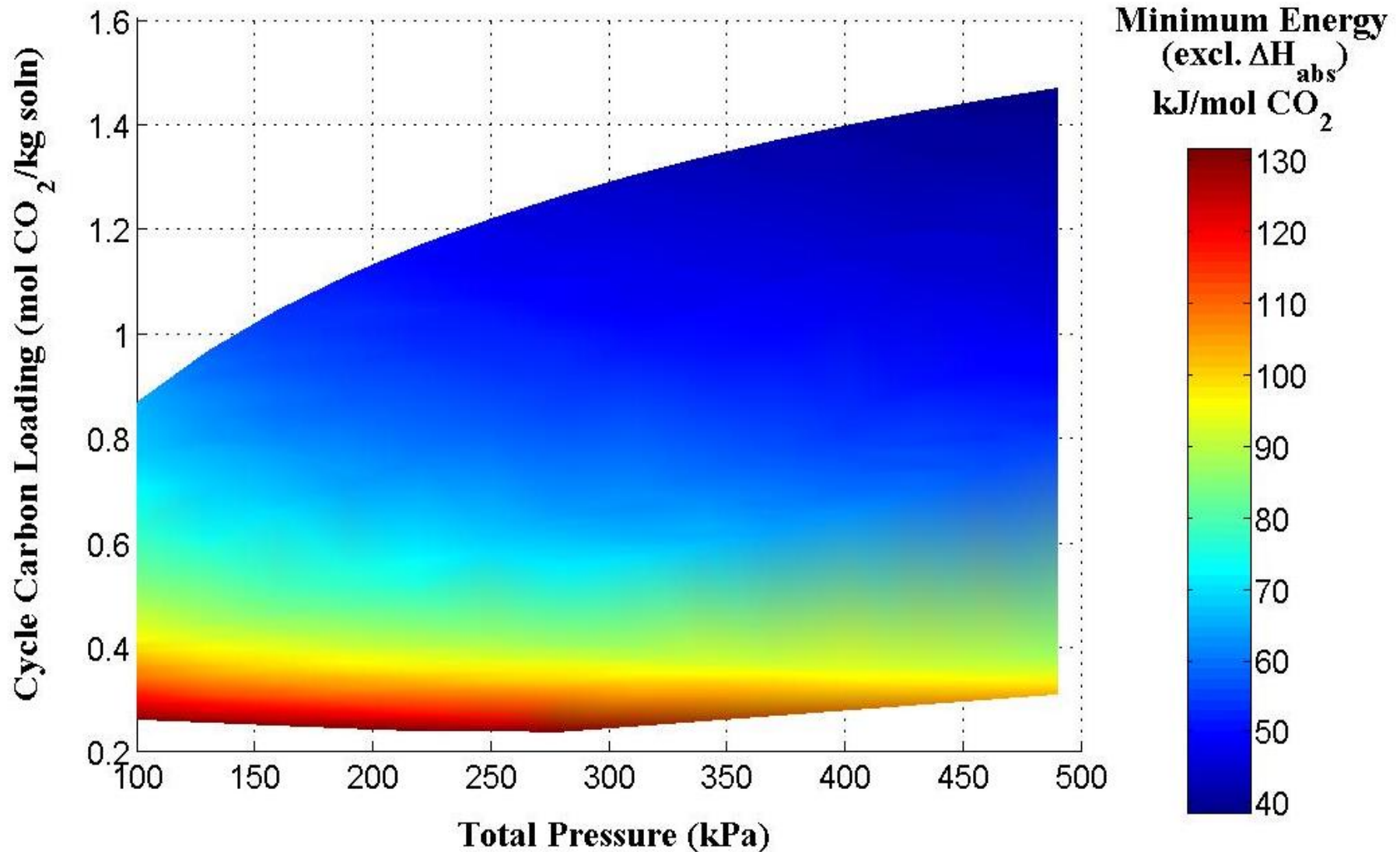
$$Q_{water\ vapor} = E_{60C} - E_{40C}$$

$$\text{Where } E_T = E_{CO_2}(T, P_{CO_2}) + E_{H_2O}$$

$$Q_{compression} = Q_{stage\ 1} + Q_{stage\ 2} + \dots$$

$$\text{Where } Q_{stage\ i} = E_{i,60C} - E_{i,40C}$$

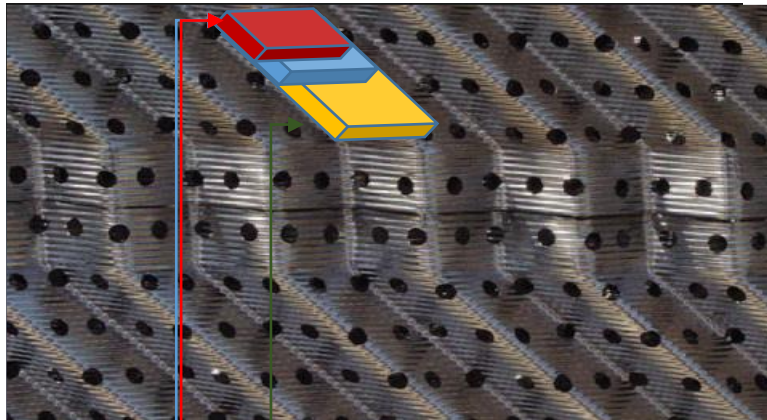
Minimum Energy Needed for Stripping and Compression for a Selected Solvent



What Does it Translate to CO₂ Flux?

- $flux = A \cdot k_G \cdot (P_{CO_2}^g - P_{CO_2}^*)$

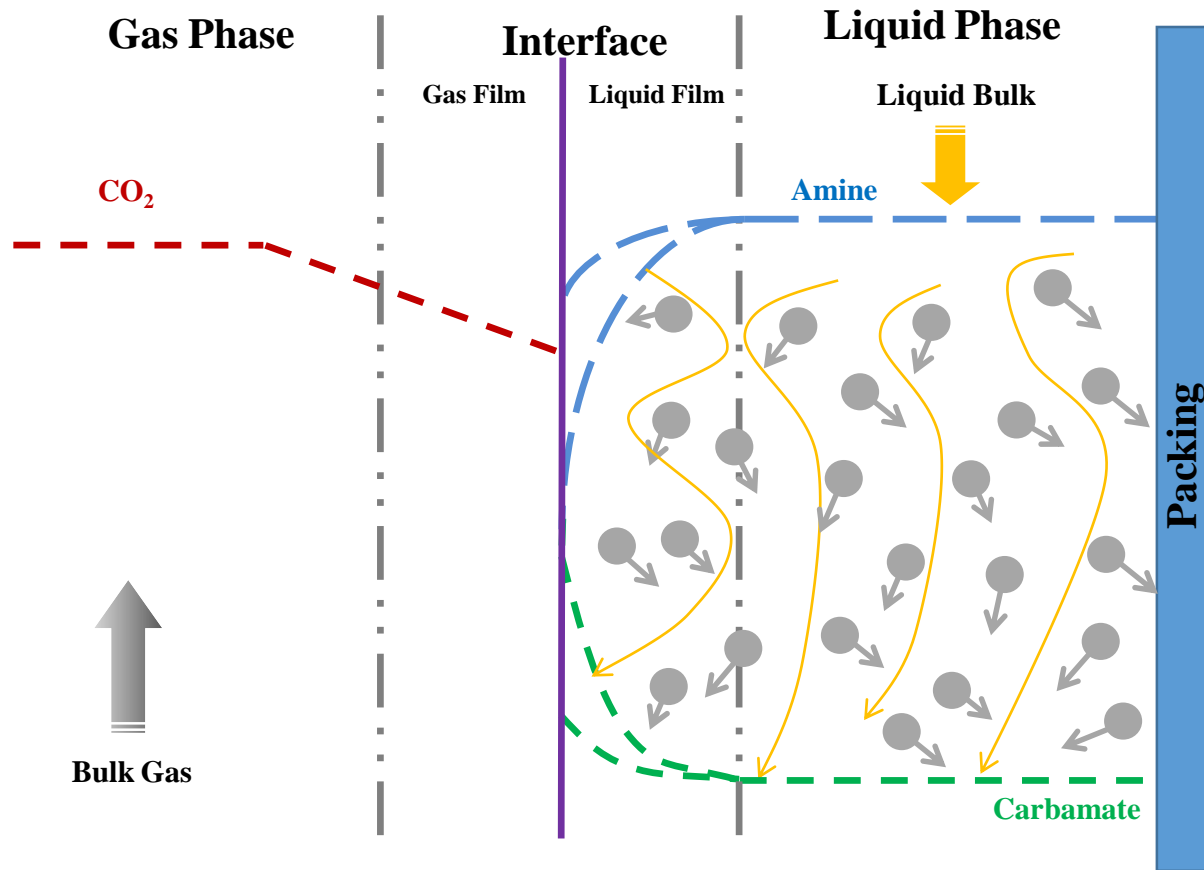
Where $k_G \propto \frac{\sqrt{D_{CO_2} \cdot k_2 \cdot [aime]}}{H_{CO_2}}$



	MEA	PZ	MDEA
Rate Constant	5.94	69.21	0.004
Self-concentrated amine	1.0	3.5	~1
Calculated Kg' impact from [M]	1	1.87	~1
Calculated Kg' impact from k ₂	1	3.41	0.03
Calculated Kg' Overall	1	6.39	0.03
Measured Mass Flux (WCC@0.1)	1	2.20	0.18

Turbulence Enhancement by Particles

➤ Turbulence Enhancement by Particles

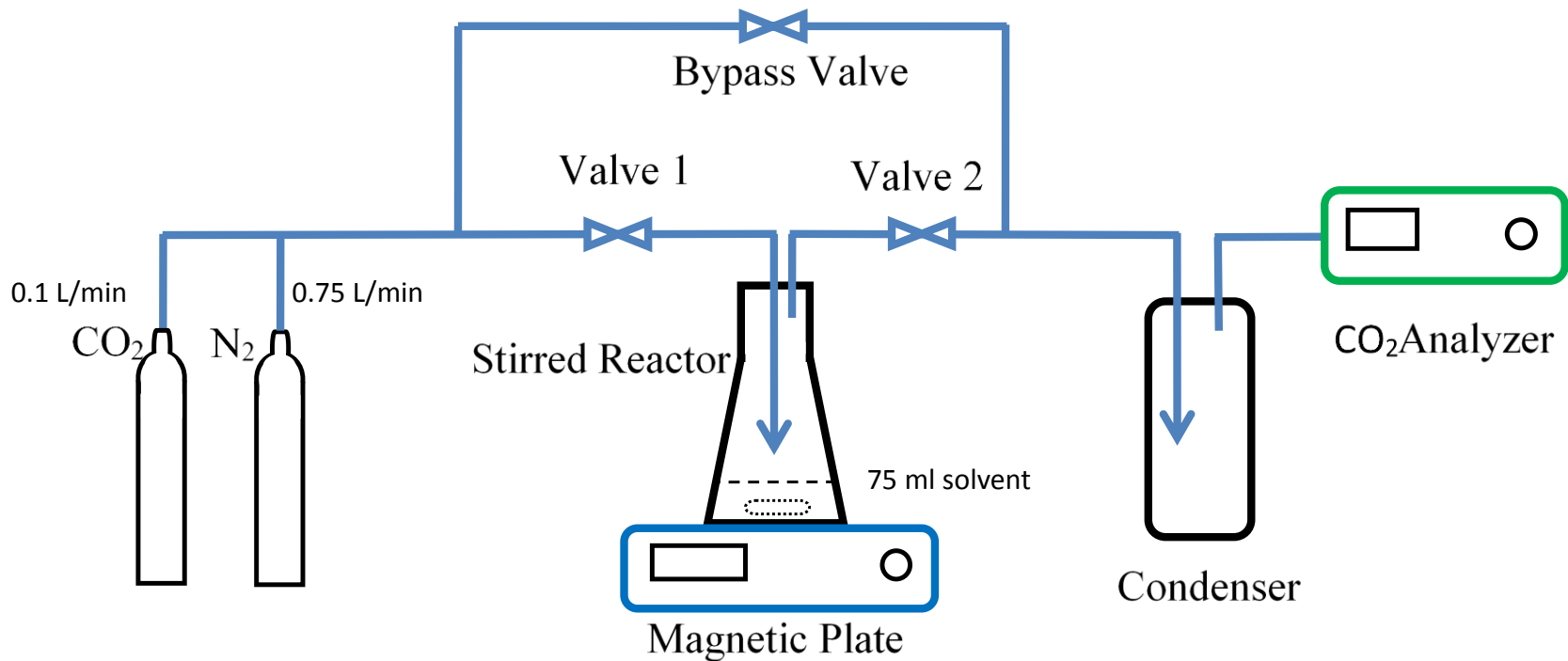


Entrained particles → Turbulence → Enhanced physical mass transfer

Mass Transfer Enhancement Experiment

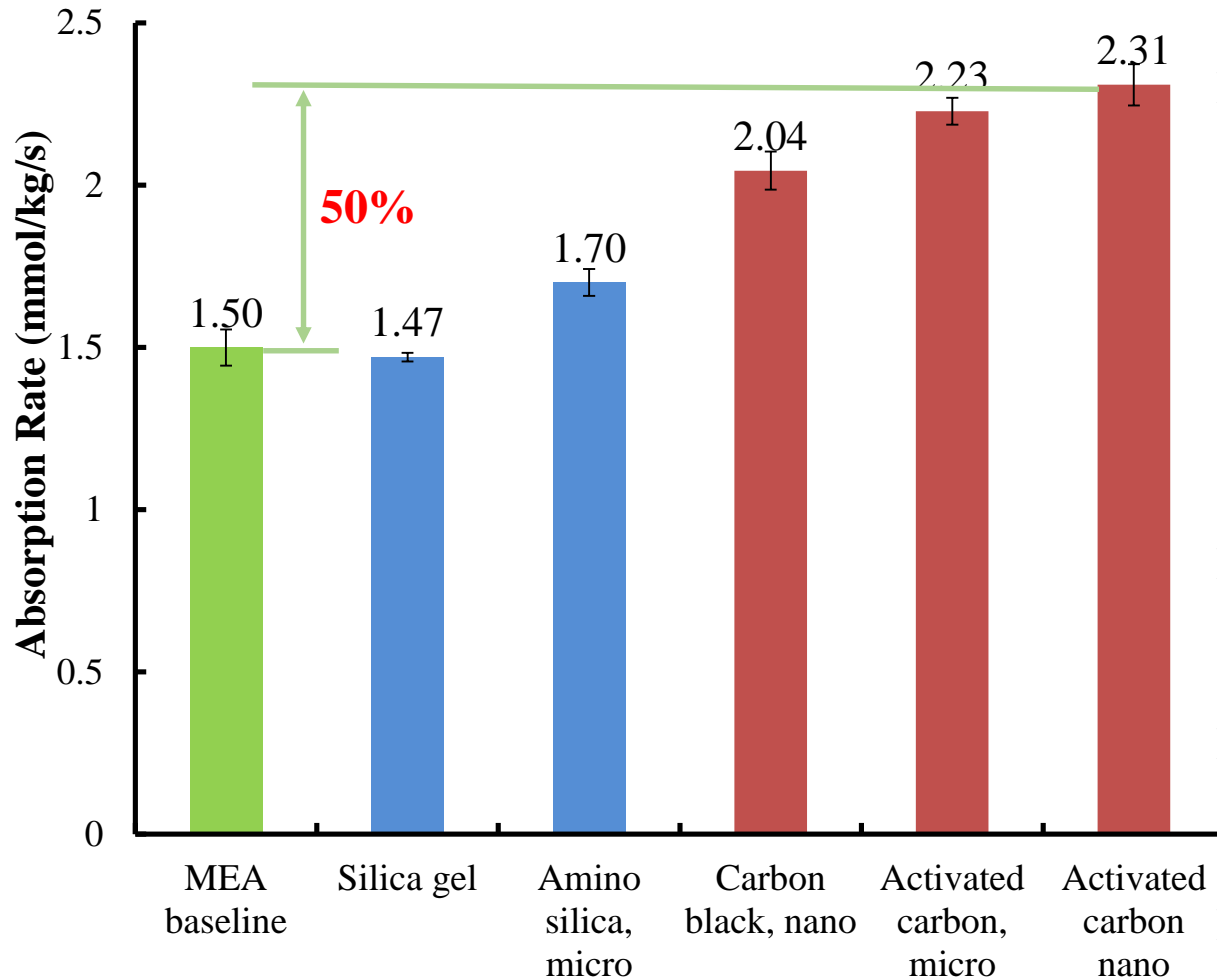
➤ Experiment Setup - Stirring Reactor with Stable Gas-Liquid Interface

Entrained particles → Turbulence → Enhanced physical mass transfer



Turbulence Enhancement by Particles

➤ Preliminary Results of Effect of Different Particles on CO₂ Absorption Enhancement



Conditions: 5M MEA with and without 1 wt % particles

➤ Hydrophilic particles potentially interact with solutions:

- ❑ Increase solution viscosity due to particle-H₂O interaction
- ❑ Decrease amine activity due to particle-amine interaction

➤ Hydrophobic particles are better than hydrophilic ones.

➤ Activated carbon particles show best enhancement (>50%).

➤ Hydrophobic particles as turbulence promoters.

Thanks and Question?